

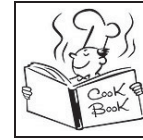
## Utility Disturbance Management in the Process Industry

Based on the PhD Thesis by Anna Lindholm

Market-driven Systems, May 22, 2014

## Utilities

*"Utilities – Support processes that are utilized in production, but are not part of the final product."*



Raw material



Equipment



Utilities



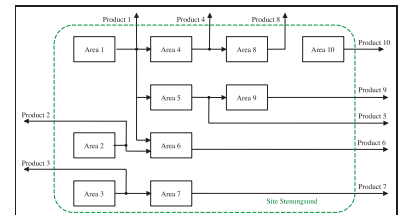
## Utilities in the process industry

*"Utilities – Support processes that are utilized in production, but are not part of the final product."*

- Steam
- Cooling water
- Electricity
- Fuel
- Water treatment
- Combustion of tail gas
- Nitrogen
- Water
- Compressed air
- Vacuum system



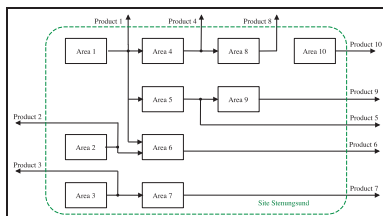
## A process industrial site



## Why disturbances in utilities?

Disturbances in utilities

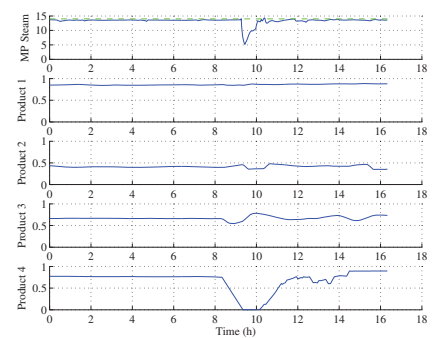
- affect many areas at a site, directly or indirectly
- are common within the process industry



Also, root cause hard to determine because of utility interdependence.

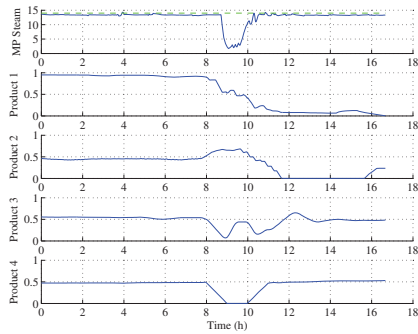
## An industrial example (1)

Example 1: Pressure drop in middle-pressure steam net



## An industrial example (2)

Example 2: Pressure drop in middle-pressure steam net



## Objective

Use a method for utility disturbance management to achieve

- ▶ information on which utilities that cause large revenue losses at a site.
- ▶ strategies for how to control the production at a disturbance to minimize the loss of revenue.

## Outline

- ▶ Disturbance management
- ▶ Disturbances in utilities
- ▶ Performance indicators
- ▶ The UDM method
- ▶ On/Off production modeling
- ▶ Matrix representation
- ▶ Case study at Perstorp
- ▶ Continuous production modeling
- ▶ Optimizing supply of utilities

## Disturbance management

### Proactive disturbance management

Disturbance management strategies that are aiming to prevent future disturbance occurrences.

### Reactive disturbance management

Disturbance management strategies for handling disturbances when they occur.

## Disturbances in utilities

No negative effect on production as long as the utility operates within limits.

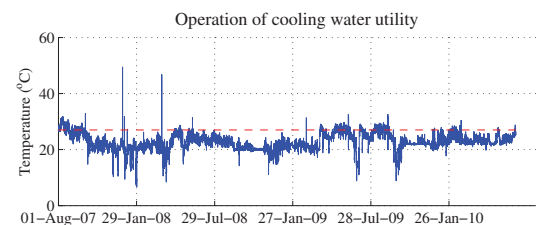
Suggestion: Set limits for when a disturbance in a utility has negative impact on the production.

- ▶ Steam: Steam pressure outside certain limits
- ▶ Cooling water: Cooling water temperature outside certain limits
- ▶ ...

⇒ Utility disturbances can be identified from measurement data.

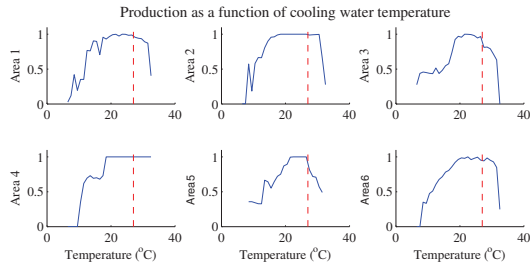
## Disturbances in utilities – Example

Example: Cooling water temperature



## Validation of limits

Example: Cooling water temperature



## Utility availability

### Definition

*Utility availability* is the fraction of time all utility parameters are inside their critical limits.

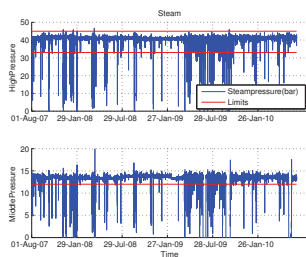
## Availability computations

Example: Steam

Disturbance limits, pressure  $p$ :

High pressure steam:  $p < 33$  bar or  $p > 45$  bar

Middle pressure steam:  $p < 12$  bar



Steam availability = 95.94 %

## Utilities required at each area

Each area at a site requires a specific set of utilities.

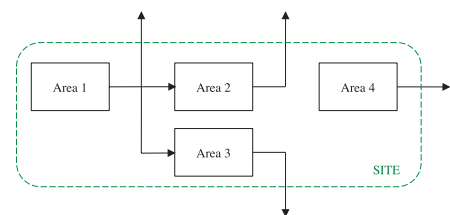
	Area 1	Area 2	Area 3	Area 4
Steam	x	x		
Cooling water	x	x	x	x
Electricity	x	x	x	x
Fuel	x			
Water treatment utility		x		x
Combustion of tail gas	x	x		
Nitrogen	x	x	x	x
Water	x	x	x	x
Compressed air	x	x	x	x
Vacuum system	x	x	x	

## Area availability

### Definition

The *direct area availability* is the fraction of time all utility parameters for all utilities needed at an area are inside their critical limits.

## Area interdependence



### Definition

The *total area availability* is the fraction of time all utility parameters for all utilities needed at an area are inside their critical limits

AND

all areas which the area is dependent on are available.

## The UDM method

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Utility Disturbance Management (UDM) method

- A) Estimate the revenue loss caused by each utility at the site
- B) Reduce the revenue loss due to future disturbances in utilities

## The UDM method – Step by step

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1. Get information on site-structure and utilities
2. Compute utility and area availabilities
3. Estimate revenue loss due to disturbances in utilities
4. Reduce revenue loss due to future disturbances in utilities

## Step 1 of the UDM method

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Get information on site structure and utilities

- a) Depict the overall structure of the site
- b) List all utilities used at the site
- c) Determine which utilities that are required at each area
- d) Draw a utility dependence flowchart
- e) Define disturbance limits for each utility
- f) Get relevant measurement data
- g) List all planned stops during the time period

## Step 2 of the UDM method

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Compute utility and area availabilities

- a) Compute utility availabilities
- b) Compute direct and total area availabilities

## Step 3 of the UDM method

---

Estimate revenue loss due to disturbances in utilities

- a) Select site model
- b) Estimate flow to the market of each product
- c) Get contribution margins for each product
- d) Estimate revenue loss for each product
- e) Estimate revenue loss due to each utility

Step 3 d) and 3 e) are dependent on the choice of modeling approach.

## Step 4 of the UDM method

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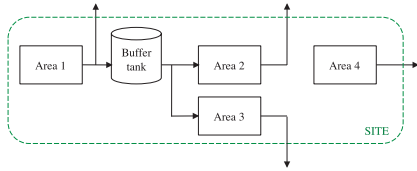
Reduce revenue loss due to future disturbances in utilities

This step is dependent on the choice of modeling approach.

The step results in

- proactive disturbance management strategies and/or
- reactive disturbance management strategies

## On/off production modeling



- Utilities and areas are considered to be either operating or not operating, i.e. 'on' or 'off'.
- An area operates at maximum production speed when available, and does not operate when not available.
- Including or not including buffer tanks between areas.

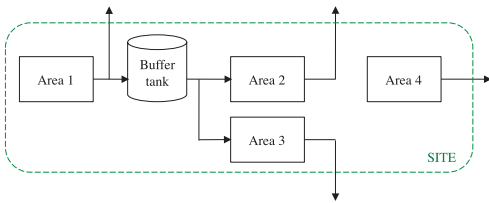
## UDM: On/off without buffer tanks

Use utility and area availabilities to estimate revenue loss

- + Simple modeling; Only need to know which utilities that are required by each area and how areas are connected
- + Orders utilities according to the revenue loss they cause
- + Worst case estimates of revenue losses
- Greatly overestimates the revenue losses
- Only information about WHICH utilities that cause large losses, no information on HOW to improve the availabilities of these utilities
- Internal buffer tanks not included  $\Rightarrow$  No decision support for choosing buffer tank levels
- No dynamics included  $\Rightarrow$  No reactive disturbance management strategies may be obtained

## Matrix representation

Representation of the interconnection of production areas



Area dependence matrix

$$A_d = \begin{bmatrix} 1 & 0 & 0 & 0 \\ 1 & 1 & 0 & 0 \\ 1 & 0 & 1 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix}$$

(size  $n_a \times n_a$ )

## Matrix representation

Representation of utility measurement data

steam =	[42	38	34	32	35	41	40	36	34	37]
cooling water =	[25	24	24	26	28	30	27	25	24	25]
electricity =	[1	1	1	1	1	1	0	1	1	1]
feed water =	[22	19	18	20	22	21	21	21	21	21]
instrument air =	[1	2	1	1	3	2	1	0	0	1]

Disturbance limits:

Steam :	pressure < 35 bar
Cooling water :	temperature > 27°C
Electricity :	on/off
Feed water :	pressure < 20 bar
Instrument air :	pressure $\leq$ 0 bar

## Matrix representation

Utility operation matrix

$$U = \begin{bmatrix} 1 & 1 & 0 & 0 & 1 & 1 & 1 & 1 & 0 & 1 \\ 1 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 1 & 1 & 1 \\ 1 & 0 & 0 & 1 & 1 & 1 & 1 & 1 & 1 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 1 \end{bmatrix}$$

(size  $n_u \times n_s$ )

## Matrix representation

Utility requirements

	Area 1	Area 2	Area 3	Area 4
Steam	x		x	
Cooling water		x	x	
Electricity	x	x	x	x
Feed water	x		x	
Instrument air	x		x	x

Area-utility matrix

$$A_u = \begin{bmatrix} 1 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 \\ 1 & 1 & 1 & 1 & 1 \\ 0 & 0 & 1 & 0 & 1 \end{bmatrix}$$

(size  $n_a \times n_u$ )



### Compute utility availability

#### Utility Availability

$$U_{av} = U \cdot \mathbf{1}/n_s$$

$$U = \begin{bmatrix} 1 & 1 & 0 & 0 & 1 & 1 & 1 & 1 & 0 & 1 \\ 1 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 1 & 1 & 1 \\ 1 & 0 & 0 & 1 & 1 & 1 & 1 & 1 & 1 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 1 \end{bmatrix} \quad U_{ud} = \begin{bmatrix} 1 & 1 & \frac{1}{2} & 0 & 1 & 1 & 1 & 1 & \frac{1}{2} & 1 \\ 1 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 & 1 \\ 1 & 0 & 0 & 1 & 1 & 1 & 1 & 1 & 1 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 1 & 1 & 0 & 1 \end{bmatrix}$$

$$U_{av} = [0.7 \quad 0.8 \quad 0.9 \quad 0.8 \quad 0.8]^T \quad U_{av}^{ud} = [0.9 \quad 0.8 \quad 0.9 \quad 0.8 \quad 0.8]^T$$

### Compute direct area availability

#### Direct area availability

$$A_{av}^{dir} = A_{dir} \cdot \mathbf{1}/n_s$$

$$A_{dir} = \mathbf{1}\mathbf{1}^T + \text{sign}(A_u(U - \mathbf{1}\mathbf{1}^T))$$

$$A_u = \begin{bmatrix} 1 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 \\ 1 & 1 & 1 & 1 & 1 \\ 0 & 0 & 1 & 0 & 1 \end{bmatrix} \quad A_u U = \begin{bmatrix} 4 & 3 & 2 & 3 & 4 & 4 & 3 & 3 & 2 & 4 \\ 2 & 2 & 2 & 2 & 1 & 1 & 1 & 2 & 2 & 2 \\ 5 & 4 & 3 & 4 & 4 & 4 & 4 & 4 & 3 & 5 \\ 2 & 2 & 2 & 2 & 2 & 2 & 1 & 1 & 1 & 2 \end{bmatrix}$$

$$A_{dir} = \begin{bmatrix} 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 1 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 \end{bmatrix}$$

### Compute direct area availability

$$A_{dir} = \begin{bmatrix} 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 1 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 \end{bmatrix}$$

$$A_{av}^{dir} = A_{dir} \cdot \mathbf{1}/n_s = [0.4 \quad 0.7 \quad 0.2 \quad 0.7]^T$$

### Compute total area availability

#### Total area availability

$$A_{av}^{tot} = A_{tot} \cdot \mathbf{1}/n_s$$

$$A_{tot} = \mathbf{1}\mathbf{1}^T + \text{sign}(A_d(A_{dir} - \mathbf{1}\mathbf{1}^T))$$

$$A_d = \begin{bmatrix} 1 & 0 & 0 & 0 \\ 1 & 1 & 0 & 0 \\ 1 & 1 & 0 & 0 \\ 0 & 0 & 0 & 1 \end{bmatrix} \quad A_d A_{dir} = \begin{bmatrix} 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 \\ 2 & 1 & 1 & 1 & 1 & 1 & 0 & 1 & 1 & 2 \\ 2 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 2 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 \end{bmatrix}$$

$$A_{tot} = \begin{bmatrix} 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 \\ 1 & \color{red}{0} & \color{red}{0} & \color{red}{0} & 0 & 0 & 0 & \color{red}{0} & \color{red}{0} & 1 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 \end{bmatrix}$$

### Compute total area availability

$$A_{tot} = \begin{bmatrix} 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \\ 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \\ 1 & 1 & 1 & 1 & 1 & 1 & 0 & 0 & 0 & 1 \end{bmatrix}$$

$$A_{av}^{tot} = A_{tot} \cdot \mathbf{1}/n_s = [0.4 \quad 0.2 \quad 0.2 \quad 0.7]^T$$

### Estimation of direct revenue loss in each area

#### Direct revenue loss in each area

$$J_p^{dir} = (\mathbf{1} - A_{av}^{dir}) \cdot q^m \cdot p n_s t_s$$

With  $q^m = [1 \quad 2 \quad 1 \quad 3]^T$ ,  $p = [1 \quad 2 \quad 4 \quad 1]^T$ ,  $t_s = 1$  we get:

$$J_p^{dir} = [6 \quad 12 \quad 32 \quad 9]^T$$

### Total revenue loss in each area

$$J_p^{tot} = \left( \mathbf{1} - A_{av}^{tot} \right) . * q^m . * pn_s t_s$$

With  $q^m = [1 \ 2 \ 1 \ 3]^T$ ,  $p = [1 \ 2 \ 4 \ 1]^T$ ,  $t_s = 1$  we get:

$$J_p^{tot} = \begin{bmatrix} 6 & 32 & 32 & 9 \end{bmatrix}^T$$

### Direct revenue loss due to utilities

$$J_u^{dir} = \text{diag} \left[ \mathbf{1} - U_{av}^{ud} \right] \cdot A_u^T(q^m \cdot * p) n_s t_s$$

$$\text{diag}[\mathbf{1} - U_{av}^{ud}] \cdot A_u^T = \begin{bmatrix} 0.1 & 0 & 0.1 & 0 \\ 0 & 0.2 & 0.2 & 0 \\ 0.1 & 0.1 & 0.1 & 0.1 \\ 0.2 & 0 & 0.2 & 0 \\ 0.2 & 0 & 0.2 & 0.2 \end{bmatrix}$$

With  $q^m = [1 \ 2 \ 1 \ 3]^T, p = [1 \ 2 \ 4 \ 1]^T, t_s = 1$ :

$$J_u^{dir} = \begin{bmatrix} 5 & 16 & 12 & 10 & 16 \end{bmatrix}^T$$

## Total revenue loss due to utilities

$$J_u^{tot} = \text{diag} [\mathbf{1} - U_{av}^{ud}] \cdot \text{sign} (A_d A_u)^T (q^m \cdot * p) n_s t_s$$

$$\text{diag} \left[ \mathbf{1} - U_{av}^{ud} \right] \cdot \text{sign} \left( A_d A_u \right)^T = \begin{bmatrix} 0.1 & 0.1 & 0.1 & 0 \\ 0 & 0.2 & 0.2 & 0 \\ 0.1 & 0.1 & 0.1 & 0.1 \\ 0.2 & 0.2 & 0.2 & 0 \\ 0.2 & 0.2 & 0.2 & 0.2 \end{bmatrix}$$

With  $q^m = [1 \ 2 \ 1 \ 3]^T$ ,  $p = [1 \ 2 \ 4 \ 1]^T$ ,  $t_s = 1$ :

$$J_u^{tot} = \begin{bmatrix} 9 & 16 & 12 & 18 & 24 \end{bmatrix}^T$$

- ▶ UDM method applied to site Stenungsund, Perstorp
- ▶ On/off production modeling without buffer tanks

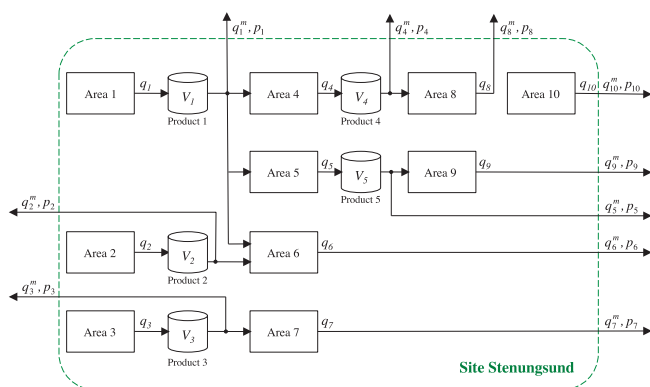


**Site Stenungsund** Located on the Swedish west coast, 50 km north of Gothenburg.

Main products: Aldehydes,  
organic acids, alcohols,  
plasticizers



## Utility requirements

[illegible]



## Summary of case study problem

- 10 production areas
- 15 utilities
- 5 internal buffer tanks
- August 1, 2007 – July 1, 2010
- Planned stop September 15 – October 8, 2009
- Sampling interval 1 minute

⇒ Size  $15 \times 1\,501\,921$  of the utility operation matrix

## Case study matrices

$$A_d = \begin{bmatrix} 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\ 1 & 0 & 0 & 1 & 0 & 0 & 0 & 0 & 0 & 0 \\ 1 & 0 & 0 & 0 & 1 & 0 & 0 & 0 & 0 & 0 \\ 1 & 1 & 0 & 0 & 0 & 1 & 0 & 0 & 0 & 0 \\ 0 & 0 & 1 & 0 & 0 & 0 & 1 & 0 & 0 & 0 \\ 1 & 0 & 0 & 1 & 0 & 0 & 0 & 1 & 0 & 0 \\ 1 & 0 & 0 & 0 & 1 & 0 & 0 & 0 & 1 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 \end{bmatrix}$$

$$A_u = \begin{bmatrix} 0 & 1 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 1 & 0 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 & 1 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 & 0 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 & 0 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 0 & 1 & 1 & 0 & 0 & 0 & 0 & 1 & 1 & 1 & 0 & 0 & 1 & 1 & 1 \\ 1 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 1 & 0 & 1 & 0 & 1 \\ 1 & 0 & 1 & 0 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 0 & 1 & 1 & 1 \\ 1 & 1 & 1 & 0 & 0 & 0 & 0 & 1 & 1 & 0 & 0 & 1 & 1 & 0 & 1 \\ 1 & 0 & 1 & 0 & 0 & 0 & 0 & 1 & 0 & 1 & 0 & 0 & 1 & 0 & 1 \end{bmatrix}$$

## Estimates of revenue losses caused by each utility

Direct loss	Total loss
Cooling water	Cooling water
MP steam	MP steam
Combustion device 9	Cooling fan 1
Combustion device 7	Feed water
Cooling fan 1	Combustion device 9
Electricity	Combustion device 7
HP steam	Electricity
Feed water	HP steam
Nitrogen	Cooling fan 2
Cooling fan 3	Cooling fan 3
Cooling fan 2	Nitrogen
Instrument air	Instrument air
Cooling fan 7	Cooling fan 7
Flare	Flare
Water treatment	Water treatment

## Case study conclusions

- The cooling water utility seems to cause the greatest losses at site Stenungsund
- Proactive disturbance management:
  - Improve availability of cooling water utility

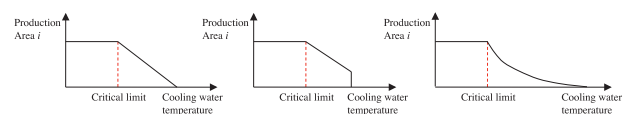
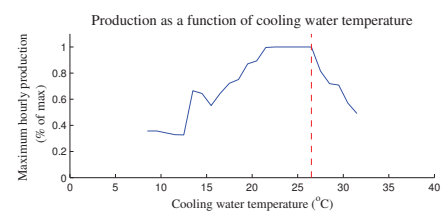
Remaining question: How should disturbances in the supply of utilities be handled, when they occur?

## Continuous production modeling

- Effects of disturbances in utilities on production
- Shared utilities (+connections of areas via the product flow)

## Continuous production modeling I

Effects of disturbances in utilities on production



## Continuous production modeling II

Connections of areas via the product flow (shared utilities)

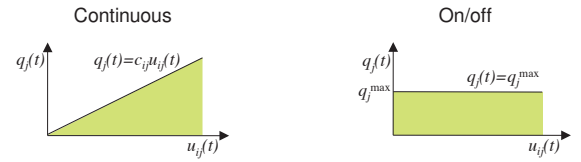


*Idea:* Separate modeling of utility effects on production from optimization problem (optimal supply of utilities to each area).'

Represent utilities as volumes that are shared by all areas that require them.

## Modeling of utilities

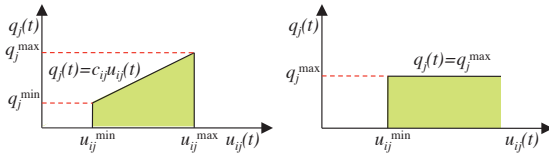
Two main types of utilities:



$$q_j \leq c_{ij}u_{ij} + m_{ij}$$

## Modeling of utilities

With maximum and minimum constraints on production:

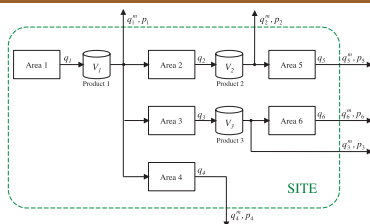


## Shared utilities

Utilities are shared between production areas:

$$\sum_j u_{ij} \leq U_i, \quad i = 1, \dots, n_u$$

## Formulation of optimization problem



Site model (mass balance)

$$V_1(t+1) = V_1(t) + q_1(t) - q_1^m(t) - q_2^{\text{in}}(t) - q_3^{\text{in}}(t) - q_4^{\text{in}}(t)$$

$$V_2(t+1) = V_2(t) + q_2(t) - q_2^m(t) - q_5^{\text{in}}(t)$$

$$V_3(t+1) = V_3(t) + q_3(t) - q_3^m(t) - q_6^{\text{in}}(t)$$

## Formulation of optimization problem

Constraints on buffer tanks

$$V_1^{\min} \leq V_1(t) \leq V_1^{\max}$$

$$V_2^{\min} \leq V_2(t) \leq V_2^{\max}$$

$$V_3^{\min} \leq V_3(t) \leq V_3^{\max}$$

### Formulation of optimization problem

#### Constraints on production rates

$$q_i^{\min} \leq q_i(t) \leq q_i^{\max}$$

or

#### Constraints on production rates

$$\begin{aligned} q_i^{\min} + s_i(t) &\leq q_i(t) \leq q_i^{\max} \\ -q_i^{\min} &\leq s_i(t) \leq 0 \end{aligned}$$

if shutdown/start-up of areas should be penalized.

### Formulation of optimization problem

Constraints due to shared utilities

$$\begin{aligned} \sum_{j \in \mathcal{M}_i} u_{ij}(t) &\leq U_i(t), \quad i = 1, \dots, n_u \\ q_j(t) &\leq c_{ij} u_{ij}(t) + m_{ij} \end{aligned}$$

#### Continuous

$$\sum_{j \in \mathcal{M}_i} \frac{1}{c_{ij}} q_j(t) - \frac{m_{ij}}{c_{ij}} \leq U_i(t)$$

#### On/off

$$q_j(t) \leq \begin{cases} q_j^{\max} & \text{if } U_i(t) = 1 \\ 0 & \text{if } U_i(t) = 0, \end{cases} \quad j \in \mathcal{M}_i$$

### Formulation of optimization problem

Area →	1	2	3	4	5	6
Steam HP	x		x			
Steam MP		x		x		x
Cooling water	x	x	x	x	x	x

Constraints due to shared utilities

$$\begin{aligned} \frac{1}{c_{11}} q_1(t) + \frac{1}{c_{13}} q_3(t) &\leq U_1(t) \\ \frac{1}{c_{22}} q_2(t) + \frac{1}{c_{24}} q_4(t) + \frac{1}{c_{26}} q_6(t) &\leq U_2(t) \\ \sum_{i=1}^6 \frac{1}{c_{3i}} q_i(t) &\leq U_3(t) \end{aligned}$$

### Formulation of optimization problem

#### Steady-state optimization

Optimal steady-state operation determined from linear program:

$$\begin{aligned} &\text{maximize } \sum_{q, q^m}^{n_a} p^T q^m \\ &\text{subject to constraints} \end{aligned}$$

⇒ Optimal profit  $p_{ref}$ , optimal production rates  $q_{ref}$ , optimal flows to market  $q_{ref}^m$  in steady state.

### Formulation of optimization problem

#### Dynamic optimization

Minimize deviation from optimal steady-state operation.

Cost function (e.g.):

$$J_t = (p^T q^m(t) - p_{ref})^2 Q_p + \Delta V^T(t) Q \Delta V(t) + \Delta q^T(t) R \Delta q(t)$$

where

$$\begin{aligned} \Delta V(t) &= V(t) - V_{ref} \\ \Delta q(t) &= q(t) - q_{ref} \end{aligned}$$

Add terms  $-g^T s(t) + s^T(t) Q_s s(t)$  if shutdown of areas should be penalized.

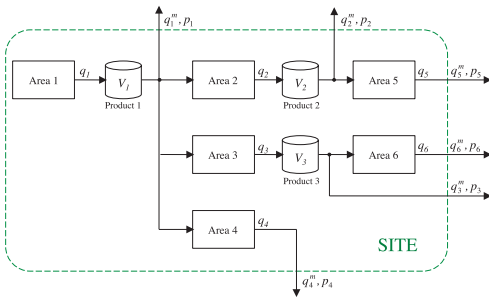
### Formulation of optimization problem

#### Dynamic optimization

$$\begin{aligned} &\text{minimize } \sum_{\tau=0}^{N-1} J_t(q(\tau), q^m(\tau), V(\tau), s(\tau)) \\ &\text{subject to constraints} \end{aligned}$$

For online disturbance management, the optimization problem may be solved in receding horizon fashion (MPC).

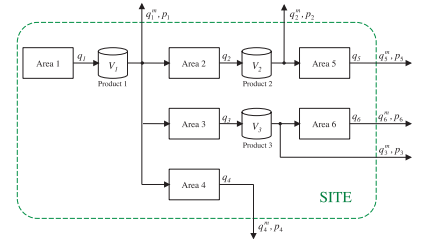
### An example



Assume utilities are shared equally at maximum production. How should utility resources be divided when a disturbance in a utility occurs?

### An example

	$q^{\max}$	$p$
Product 1	1	0.4
Product 2	0.5	0.7
Product 3	0.2	0.1
Product 4	0.1	0.5
Product 5	0.2	0.8
Product 6	0.2	1.0



Solution to steady state optimization problem

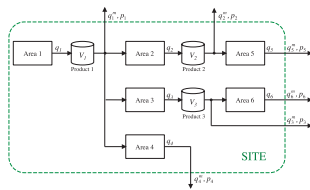
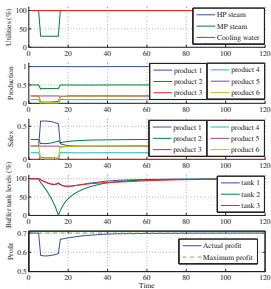
$$q_{\text{ref}} = [1 \quad 0.5 \quad 0.2 \quad 0.1 \quad 0.2 \quad 0.2]^T$$

$$q_{\text{ref}}^m = [0.2 \quad 0.3 \quad 0 \quad 0.1 \quad 0.2 \quad 0.2]^T$$

with the optimal profit  $p_{\text{ref}} = 0.7$ .

### Solution to dynamic optimization problem

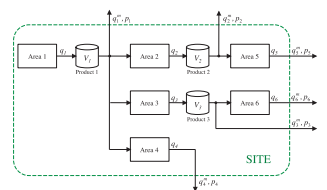
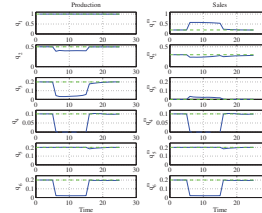
MP steam disturbance



MP steam affects area 2, 4 and 6.

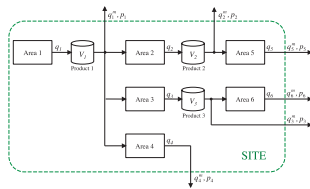
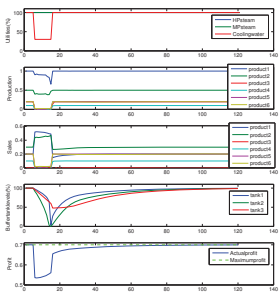
### Solution to dynamic optimization problem

MP steam disturbance



### Solution to dynamic optimization problem

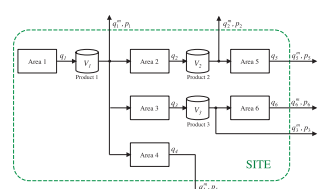
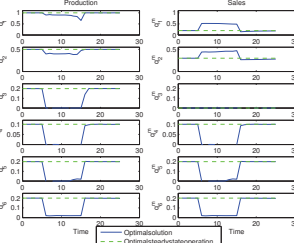
Cooling water disturbance



Cooling water affects all areas.

### Solution to dynamic optimization problem

Cooling water disturbance



## UDM: Continuous production modeling

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Continuous representation of utilities and areas.

- + Find and evaluate reactive disturbance management strategies
- + Process understanding by simulations
- + MPC as a tool for online disturbance management
- Much modeling effort needed
- Could be hard to identify utilities effect on production

## Summary

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- ▶ Disturbances in utilities cause great losses at industrial sites.
- ▶ Their effect is hard to predict since they are shared between production areas, that are connected by the product flow.
- ▶ The UDM method is a general method for utility disturbance management.
- ▶ The UDM method with on/off production modeling is a tool for quickly ordering the utilities at a site according to the loss they cause. The computations can be carried out efficiently using a matrix representation.
- ▶ The UDM method with continuous production modeling gives both proactive and reactive disturbance management strategies. MPC may be used for online disturbance management.

## Documentation

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- ▶ A General Method for Handling Disturbances on Utilities in the Process Industry, Anna Lundholm, Hampus Carlsson, Charlotta Johnsson, 18th IFAC World Congress, Milano, Italy, 2011 (the general idea, motivation)
- ▶ A Tool for Utility Disturbance Management, Anna Lundholm, Charlotta Johnsson, 14th IFAC Symposium on Information Control Problems in Manufacturing, Bucharest, Romania, May 2012 (the on/off model case)
- ▶ Formulating an Optimization Problem for Minimization of Losses due to Utilities, Anna Lindholm, Pontus Giselsson, International Symposium on Advanced Control of Chemical Processes, Singapore, July 2012. (the continuous model case)