# Feedback – An Example, Stability, Stationary Errors

Automatic Control, Basic Course, Lecture 4

November 15, 2017

Lund University, Department of Automatic Control

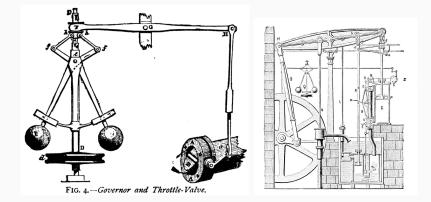
1. Feedback – The Steam Engine

2. Stability

3. Stationary Errors

# Feedback – The Steam Engine

#### Control in the Old Days



James Watt (1788): centrifugal/fly-ball governor for steam engines (based on Huygens work on windmills).

Watt earlier improved performance for steam engines with "condenser".

#### The Uncontrolled Steam Engine



Model:

$$J\dot{\omega} + D\omega = M_d - M_I$$

The stationary angular speed:

$$\omega_s = \frac{M_d - M_l}{D}$$

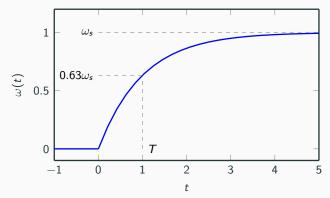
#### The Uncontrolled Steam Engine

Step response:

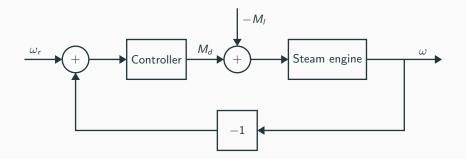
$$\omega(t) = \frac{M_d - M_l}{D} \left( 1 - e^{-Dt/J} \right) = \omega_s \left( 1 - e^{-Dt/J} \right)$$

Time constant:

$$T = \frac{J}{D}$$



### P Control of the Steam Engine



Proportional control:

$$M_d = K(\omega_r - \omega)$$

#### P Control of the Steam Engine

Dynamics with P-controller:

$$J\dot{\omega} + D\omega = \overbrace{\mathcal{K}(\omega_r - \omega)}^{M_d} - M_I$$

or

$$J\dot{\omega} + (D+K)\omega = K\omega_r - M_I$$

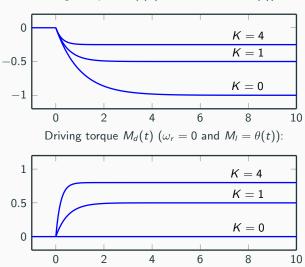
In stationarity ( $\dot{\omega} = 0$ ):

$$\omega_s = \frac{K}{D+K}\omega_r - \frac{1}{D+K}M_l$$

Step response ( $\omega(0) = 0$ ):

$$\omega(t) = \frac{K\omega_r - M_b}{D + K} \left( 1 - e^{-(D + K)t/J} \right) = \omega_s \left( 1 - e^{-(D + K)t/J} \right)$$

#### P Control of the Steam Engine



Angular speed  $\omega(t)$  ( $\omega_r = 0$  and  $M_l = \theta(t)$ ):

Introduce a PI-controller to get rid of the stationary error:

$$M_d = K(\omega_r - \omega) + rac{K}{T_i} \int_0^t (\omega_r - \omega) \mathrm{d} au$$

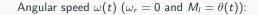
Dynamics:

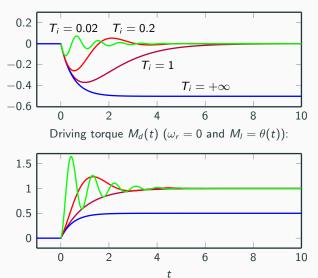
$$J\dot{\omega} + D\omega = K(\omega_r - \omega) + \frac{K}{T_i} \int_0^t (\omega_r - \omega) d\tau - M_l$$
$$J\ddot{\omega} + D\dot{\omega} = K(\dot{\omega}_r - \dot{\omega}) + \frac{K}{T_i} (\omega_r - \omega) - \dot{M}_l$$

At stationarity ( $\dot{\omega}_r = 0$ ,  $\dot{M}_l = 0$ ):

$$\omega_s = \omega_r$$

#### **PI Control of the Steam Engine**





The Laplace transformation of the dynamics

$$J\ddot{\omega} + D\dot{\omega} = K(\dot{\omega}_r - \dot{\omega}) + rac{K}{T_i}(\omega_r - \omega) - \dot{M}_l$$

is

$$s^{2}J\omega + sD\omega = K(s\omega_{r} - s\omega) + \frac{K}{T_{i}}(\omega_{r} - \omega) - sM_{i}$$

The characteristic equation (the equation to determine the poles) is:

$$s^2 + \frac{D + K}{J}s + \frac{K}{J T_i} = 0$$

By choosing K and  $T_i$ , we can place the poles of the closed loop dynamics arbitrarily.

## Stability

#### **Stability - Definitions**

A system on state space form

$$\dot{x} = Ax + Bu$$
$$y = Cx + Du$$

is

Asymptotically stable if  $x(t) \rightarrow 0$  when  $t \rightarrow +\infty$  for all initial states x(0) when u(t) = 0.

**Stable** if x(t) is bounded for all t and all initial states x(0) when u(t) = 0.

**Unstable** if x(t) grows unbounded for an initial state x(0) when u(t) = 0.







biking on convex cobble-

### **Stability - Definitions**

A system on state space form

 $\dot{x} = Ax + Bu$ y = Cx + Du

is

Asymptotically stable if  $x(t) \rightarrow 0$  when  $t \rightarrow +\infty$  for all initial states x(0) when u(t) = 0.

**Stable** if x(t) is bounded for all t and all initial states x(0) when u(t) = 0.

**Unstable** if x(t) grows unbounded for an initial state x(0) when u(t) = 0.







#### For the scalar case

$$\dot{x}(t) = ax(t)$$
  
 $x(0) = x_0$ 

the solution is:

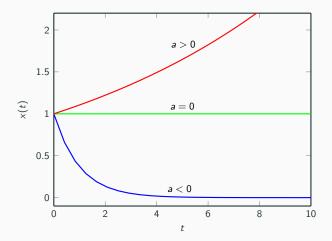
$$x(t) = e^{at} \cdot x_0$$

Hence

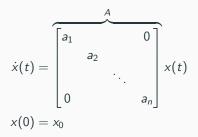
- a < 0 Asymptotically stable
- a = 0 (marginally) Stable
- a > 0 Unstable

### Stability - Scalar Case

$$\dot{x}(t) = ax(t), \quad x(0) = 1$$



#### **Stability - Diagonal Case**



Every state variable corresponds to the scalar case:

 $\dot{x}_i(t) = a_i x_i(t)$ 

In fact, the  $a_i$ 's are **eigenvalues of** A. The system is

**Asymptotically stable** if all the eigenvalues of *A* have negative real part **Unstable** if at least one of the eigenvalues of *A* has a positive real part (marginally) **Stable** if all the eigenvalues of *A* have either negative or zero real part

#### Stability - General Case

For a general A-matrix, i.e., not necessarily a diagonal one, the stability rule still holds with one exception, namely that the eigenvalues having zero real part do not always guarantee stability, unless the purely imaginary eigenvalues are unique

Example

$$A = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}$$

has a **double eigenvalue** at  $\lambda = 0$ .

#### Stability - General Case

For a general A-matrix, i.e., not necessarily a diagonal one, the stability rule still holds with one exception, namely that the eigenvalues having zero real part do not always guarantee stability, unless the purely imaginary eigenvalues are unique

Example

$$A = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}$$

has a **double eigenvalue** at  $\lambda = 0$ .

The differential equation  $\dot{x} = Ax$  has the solution

$$x(t) = e^{\begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}^{t}} x(0) = \begin{bmatrix} 1 & t \\ 0 & 1 \end{bmatrix} \begin{bmatrix} x_{1}(0) \\ x_{2}(0) \end{bmatrix} = \begin{bmatrix} x_{1}(0) + x_{2}(0) \cdot t \\ x_{2}(0) \end{bmatrix}$$

which **grows unbounded** for any  $x_2(0) \neq 0$ ;

#### **Stability - Transfer Function**

Recall from Lecture 2 that the eigenvalues of the A matrix are poles to the transfer function. Hence, if all the poles have negative real part the system is stable.

A second order polynomial

$$s^2 + a_1 s + a_2$$

has its roots in the left half plane if and only if  $a_1 > 0$  and  $a_2 > 0$ . A third order polynomial

$$s^3 + a_1s^2 + a_2s + a_3$$

has its roots in the left half plane if  $a_1 > 0$ ,  $a_2 > 0$ ,  $a_3 > 0$  and

 $a_1a_2 > a_3$ 

#### **Stability - Transfer Function**

Recall from Lecture 2 that the eigenvalues of the A matrix are poles to the transfer function. Hence, if all the poles have negative real part the system is stable.

A second order polynomial

$$s^2 + a_1s + a_2$$

has its roots in the left half plane if and only if  $a_1 > 0$  and  $a_2 > 0$ .

A third order polynomial

$$s^3 + a_1 s^2 + a_2 s + a_3$$

has its roots in the left half plane if  $a_1 > 0$ ,  $a_2 > 0$ ,  $a_3 > 0$  and

 $a_1 a_2 > a_3$ 

Stability critera wrt coeffients can be derived with **Routh-Hurwitz criterion**.

#### Example

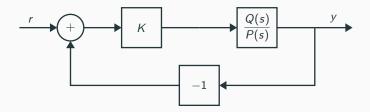
Determine if the systems below are asymptotically stable or not

a)  $G(s) = \frac{1}{(s^2 + s + 1)(s + 1)}$  b)

$$\dot{x} = \begin{bmatrix} -2 & 2\\ 0 & -3 \end{bmatrix} x + \begin{bmatrix} 1\\ 1 \end{bmatrix} u$$
$$y = \begin{bmatrix} 2 & -1 \end{bmatrix} x + 2u$$

#### **Root Locus**

Idea: Study graphically how the poles move with the change of a parameter



$$Y(s) = \frac{KQ(s)}{P(s) + KQ(s)}R(s)$$

Characteristic equation:

P(s) + KQ(s) = 0

#### **Root Locus**

Characteristic equation:

$$P(s) + KQ(s) = 0$$

For K = 0 the characteristic equation becomes:

P(s)=0

When  $K \to \infty$ , the characteristic equation becomes:

Q(s) = 0

i.e., the poles of the closed loop system will approach the zeros of the closed loop system.

If there are more poles than zeros, the remaining poles will approach infinity (in magnitude).

Let

$$\frac{Q(s)}{P(s)} = \frac{1}{s(s+1)}$$

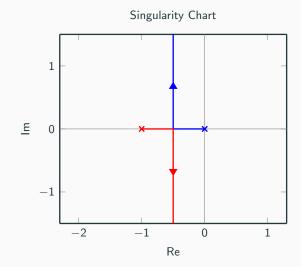
Characteristic equation of the closed loop:

$$P(s) + KQ(s) = s(s+1) + K = 0$$
$$s = -\frac{1}{2} \pm \sqrt{\frac{1}{4} - K}$$

When K = 0, poles in 0, -1.

When K > 1/4, complex pair of poles with real part -1/2. The imaginary parts go towards  $\pm \infty$  when  $K \rightarrow \infty$ .

## Root Locus - Second Order System

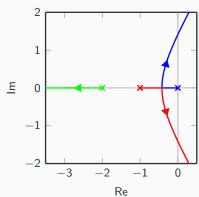


Let

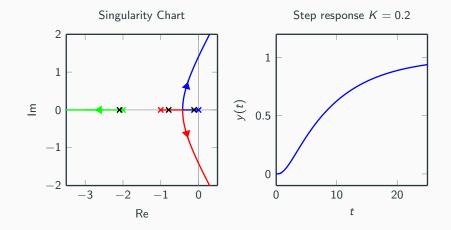
$$\frac{Q(s)}{P(s)} = \frac{1}{s(s+1)(s+2)}$$

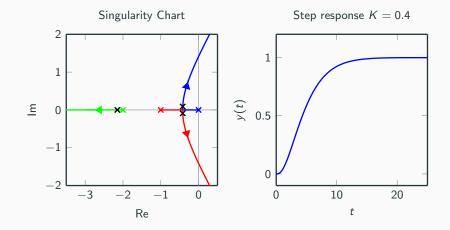
Characteristic equation of the closed loop:

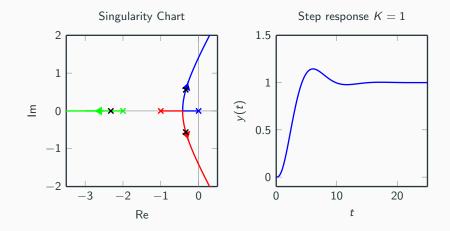
$$P(s) + KQ(s) = s(s+1)(s+2) + K = s^3 + 3s^2 + 2s + K = 0$$

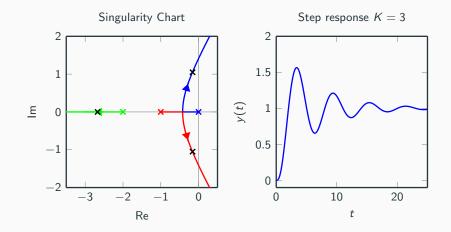


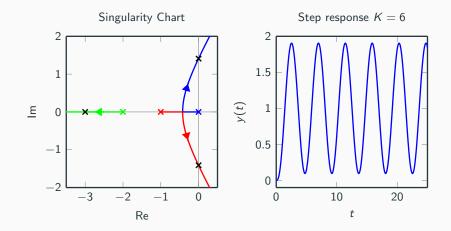
Singularity Chart

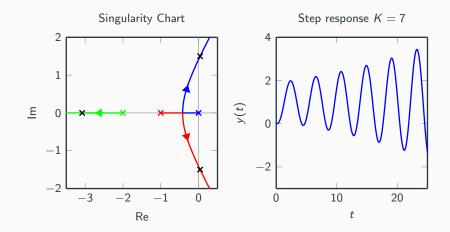






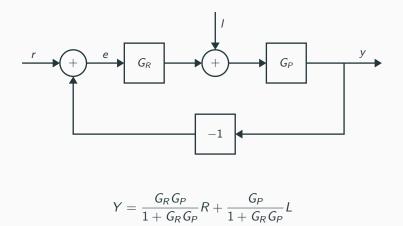






## **Stationary Errors**

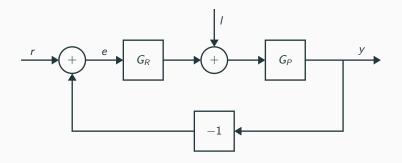
## The Servo Problem and The Regulator Problem



**The Servo Problem** Set point tracking of  $\mathbf{r}$ , (l = 0).

The Regulator Problem Effect of load disturbances I, (r = 0).

## The Servo Problem and The Regulator Problem



$$Y = \frac{G_R G_P}{1 + G_R G_P} R + \frac{G_P}{1 + G_R G_P} L$$

The Servo Problem Set point tracking of  $\mathbf{r}$ , (l = 0).

The Regulator Problem Effect of load disturbances I, (r = 0).

Use **superposition property** of linear systems to consider them **separately**.

$$E(s) = R(s) - Y(s) = \frac{1}{1 + \underbrace{G_R(s)G_P(s)}_{G_0(s)}}R(s)$$

We can use the final value theorem to determine the error

$$e_{\infty} = \lim_{t \to +\infty} e(t) = \lim_{s \to 0} sE(s)$$

but only if sE(s) has it poles strictly in the left half plane.

Let the process and controller be:

$$G_P = rac{1}{s(1+sT)}$$
  $G_R = K$ 

Open-loop transfer function:

$$G_0 = G_R G_P = \frac{K}{s(s+sT)}$$

The control error is given by:

$$E(s) = \frac{1}{1 + G_0(s)}R(s) = \frac{s(1 + sT)}{s(1 + sT) + K}R(s)$$

The control error is given by:

$$E(s) = \frac{1}{1 + G_0(s)}R(s) = \frac{s(1 + sT)}{s(1 + sT) + K}R(s)$$

Let r(t) be a step, i.e.,

$$r(t) = egin{cases} 1 & ext{if } t \geq 0 \ 0 & ext{if } t < 0 \end{cases} \quad R(s) = rac{1}{s}$$

Then (given that T and K are positive)

$$e_{\infty} = \lim_{t \to +\infty} e(t) = \lim_{s \to 0} sE(s) = \lim_{s \to 0} s \cdot \frac{s(1+sT)}{s(1+sT)+K} \cdot \frac{1}{s} = 0$$

The control error is given by:

$$E(s) = \frac{1}{1 + G_0(s)}R(s) = \frac{s(1 + sT)}{s(1 + sT) + K}R(s)$$

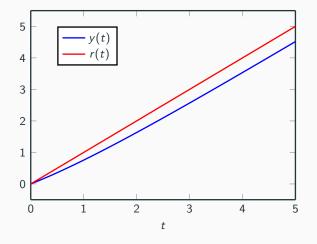
Let r(t) be a ramp, i.e.,

$$r(t) = \begin{cases} t & \text{if } t \ge 0 \\ 0 & \text{if } t < 0 \end{cases} \quad R(s) = \frac{1}{s^2}$$

Then (given that T and K are positive)

$$e_{\infty} = \lim_{t \to +\infty} e(t) = \lim_{s \to 0} sE(s) = \lim_{s \to 0} s \cdot \frac{s(1+sT)}{s(1+sT)+K} \cdot \frac{1}{s^2} = \frac{1}{K}$$

# Stationary Errors - The Servo Problem - Example



Question to the audience: What value of K is used?

Open loop transfer function:

$$G_0(s) = \frac{K}{s^n} \cdot \frac{1 + b_1 s + b_2 s^2 + \dots}{1 + a_1 s + a_2 s^2 + \dots} e^{-sL} = \frac{KB(s)}{s^n A(s)} e^{-sL}$$

Set point (*m* non-negative integer):

$$r(t) = \begin{cases} \frac{t^m}{m!} & \text{if } t \ge 0\\ 0 & \text{if } t < 0 \end{cases} \quad R(s) = \frac{1}{s^{m+1}}$$

Error (given that the limit exists):

$$e_{\infty} = \lim_{t \to +\infty} e(t) = \lim_{s \to 0} s \cdot \frac{s^n A(s)}{s^n A(s) + KB(s)e^{-sL}} \cdot \frac{1}{s^{m+1}} = \lim_{s \to 0} \frac{1}{s^n + K} s^{n-m}$$

The stationary error is determined by the low-frequency properties of the transfer function and the set point.

$$G_0(s) = \frac{K}{s^n} \cdot \frac{1 + b_1 s + b_2 s^2 + \dots}{1 + a_1 s + a_2 s^2 + \dots} e^{-sL} = \frac{KB(s)}{s^n A(s)} e^{-sL}$$
$$r(t) = \begin{cases} \frac{t^m}{m!} & \text{if } t \ge 0\\ 0 & \text{if } t < 0 \end{cases}$$

The relation between m and n gives the following errors:

$$\begin{array}{ll} n > m & e_{\infty} = 0 \\ n = m = 0 & e_{\infty} = \frac{1}{1+K} \\ n = m \ge 1 & e_{\infty} = \frac{1}{K} \\ n < m & \text{Limit does not exist} \end{array}$$

The transfer function between a load disturbance I(t) and measurement signal y(t):

$$Y(s) = \frac{G_P(s)}{1 + G_R(s)G_P(s)}L(s)$$

Since r = 0, we can study the measurement signal instead of the error:

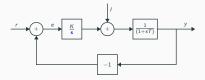
$$y_{\infty} = \lim_{t \to +\infty} y(t) = \lim_{s \to 0} sY(s)$$

Again, we have to ensure that the limit exists.

## Stationary Errors - The Regulator Problem - Example

Let the controller and process be:

$$G_P = rac{1}{1+sT}, \qquad G_R = rac{K}{s}$$



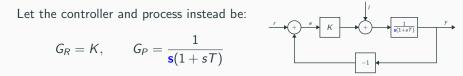
Let the load disturbance I(t) be a step:

$$U(t) = egin{cases} 1 & ext{if } t \geq 0 \ 0 & ext{if } t < 0 \end{cases}$$

The final theorem yields:

$$y_{\infty} = \lim_{t \to +\infty} y(t) = \lim_{s \to 0} s \cdot \frac{\mathbf{s}}{\mathbf{s}(1 + sT) + K} \cdot \frac{1}{s} = 0$$

### Stationary Errors - The Regulator Problem - Example



Notice that  $G_0 = G_P G_R$  is the same as in the previous slide. Let the load disturbance I(t) be a step:

$$\mathcal{U}(t) = egin{cases} 1 & ext{if } t \geq 0 \ 0 & ext{if } t < 0 \end{cases}$$

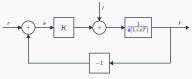
The final theorem yields:

$$y_{\infty} = \lim_{t \to +\infty} y(t) = \lim_{s \to 0} s \frac{1}{\mathbf{s}(1+sT) + K} \cdot \frac{1}{s} = \frac{1}{K}$$

## Stationary Errors - The Regulator Problem - Example

Let the controller and process instead be:

$$G_R = K, \qquad G_P = rac{1}{\mathbf{s}(1+sT)}$$



Notice that  $G_0 = G_P G_R$  is the same as in the previous slide. Let the load disturbance I(t) be a step:

$$l(t) = egin{cases} 1 & ext{if } t \geq 0 \ 0 & ext{if } t < 0 \end{cases}$$

The final theorem yields:

$$y_{\infty} = \lim_{t \to +\infty} y(t) = \lim_{s \to 0} s \frac{1}{\mathbf{s}(1+sT) + K} \cdot \frac{1}{s} = \frac{1}{K}$$

In the regulator problem, the placement of integrators matters (i.e., if integrators are in controller or in plant).

## Stationary Errors - The Regulator Problem - General Case

Let

$$G_P(s) = \frac{K_P B_P(s)}{s^p A_p(s)} e^{-sL} \quad G_R(s) = \frac{K B_R(s)}{s^r A_R(s)}$$

where  $A_P(0) = B_P(0) = A_R(0) = B_R(0) = 1$ . Moreover, let the load disturbances be given by

$$L(s) = \frac{1}{s^{m+1}}$$

Then

$$y_{\infty} = \lim_{s \to 0} \frac{K_P}{s^{r+p} + KK_P} s^{r-m}$$

The stationary becomes (given that the limits exists):

$$\begin{array}{ll} r > m & y_{\infty} = 0 \\ r = m = 0, \ p = 0 & y_{\infty} = \frac{K_P}{1 + KK_P} \\ r = m = 0, \ p \ge 0 & y_{\infty} = \frac{1}{K} \\ r = m \ge 1 & y_{\infty} = \frac{1}{K} \\ r < m & \text{The limit does not exist.} \end{array}$$

#### Example

The transfer function of a process is

$$G_p(s)=rac{1}{s+1}.$$

The process is controlled with a PI-regulator,

$$G_r(s)=1+\frac{2}{s}.$$

The closed loop system is able to follow step changes in the reference value without any stationary error, but when the reference is a ramp-signal, r(t) = ct, a stationary error emerges. Determine the magnitude of this stationary error.